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2 3	Wind turbine, waste, and material recovery
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A circular economy approach to green energy: Wind turbine, waste, and material recovery

HIGHLIGHTS

- Four economic preconditions ensure re-entry of recovered fiber into circular system
- Rapid heating rate and high temperature reduce char formation on carbon fiber
- Effect of inert gas flow on reduction of char residues is only obvious at 550°C
- Improved pyrolysis conditions increase char intrinsic reactivity and oxidation rate

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2 material recovery

3 ABSTRACT

4 Wind energy has been considered as one of the greenest renewable energy sources over the last two decades. However, attention is turning to reducing the possible environmental 5 impacts from this sector. We argue that wind energy would not be effectively "green" if 6 7 anthropogenic materials are not given attention in a responsible manner. Using the concept of the circular economy, this paper considers how anthropogenic materials in the form of carbon 8 fibers can reenter the circular economy system at the highest possible quality. This paper first 9 10 investigates the viability of a carbon-fiber-reinforced polymer extraction process using thermal pyrolysis to recalibrate the maximum carbon fiber value by examining the effect of 11 12 (a) heating rate, (b) temperature, and (c) inert gas flow rate on char yield. With cleaner and higher quality recovered carbon fibers, this paper discusses the economic preconditions for 13 the takeoff and growth of the industry and recommends the reuse of extracted carbon fibers to 14 close the circular economy loop. 15

16 HIGHLIGHTS

Four economic preconditions ensure re-entry of recovered fiber into circular system
Rapid heating rate and high temperature reduce char formation on carbon fiber
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Improved pyrolysis conditions increase char intrinsic reactivity and oxidation rate *Keywords:*

22 circular economy, wind turbine, carbon fiber, pyrolysis, recovery, recycling

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24 1. Introduction

Wind energy has been considered as one of the greenest renewable energy sources over 25 the last two decades (Liu and Barlow 2017; Liu et al., 2019). As a result, national and 26 regional energy policies have encouraged the development of onshore and offshore wind 27 farms, where installed capacity has grown rapidly from 7,600 MW in 1998 to 591,000 MW in 28 2018 (Global Wind Energy Council [GWEC], 2015; 2019). Amidst this growth, attention 29 turns naturally to the environmental impact of end-of-life turbine blades, especially when the 30 end-of-life blades and associated structures end up in landfills and negate the "green" 31 32 credentials of the industry.

This is a pertinent challenge because the annualized growth rate in wind power over the 33 first decade of the 21st century exceeded 12% (GWEC, 2014) and based on projection, 14.9-34 18% of global electricity demands will be supplied by wind energy between 2020 and 2050 35 (European Wind Energy Association [EWEA], 2014; International Energy Association 36 37 [IEA], 2011). A steady growth scenario of new installation wind farms around the world has been reported by Liu and Barlow (2017) in China, the United States, Europe, and the rest of 38 the world, as shown in Fig. 1. New global installation capacity grew to 51.7 GW in 2014, 39 40 then 63.8 GW in 2015 but stayed fairly consistent for the next 3 years (54.9 GW in 2016, 53.5 GW in 2017, and 51.3 GW in 2018) in a report by the GWEC (2019). 41

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----- INSERT FIGURE 1 HERE -----

With the rapid growth in wind energy capacities, and considering the typical turbine
design lifespan of 20 years, Liu and Barlow (2017) have projected that the end-of-life waste
from turbines becomes a critical global problem by 2028. Albers (2009) predicted around
50,000 tons of blade waste in 2020, with the amount exceeding 200,000 tons by 2034.
Similarly, Andersen et al. (2014) predicted 400,000 tons of blade waste being generated

between 2029 and 2033. Liu and Barlow (2017) estimate the blade material usage in China
reaching 1,500,000 tons by 2050. Therefore, there is a pressing need to consider this very
significant waste stream.

A typical horizontal-axis unit consists of four main components: a foundation, a tower, a nacelle, and three blades. The nacelle is fabricated from steel and copper. The tower is fabricated from concrete or steel and the foundation is made solely from concrete, with the rotating blades made from composite materials to minimize inertial and windage losses. Considering the anthropogenic materials used, composite is one of the most problematic materials because there are currently no mature recycling channels (Job, 2013; Pimenta and Pinho, 2011).

58 The composite found in the blades is of fiber-reinforced polymer composite for ease of 59 manufacture into aerodynamic shape and high mechanical performance. However, because of the cross-linked polymer chains in the thermoset matrix, recycling remains a significant 60 61 challenge, particularly reusing the ingredients in other high-grade applications. Most of the older blades are made of glass-fiber-reinforced polymer (GFRP) composites because of their 62 relatively low manufacturing and material costs. However, this imposes a constraint for 63 64 recycling options because cost must be tightly controlled to make the recycling process economically viable. To date, the only recycling route that is commercially active is where 65 GFRP waste is shredded and consumed in cement kilns. The value of the waste stream is 66 reduced to that of calcium carbonate, making this approach only viable where landfill is 67 prohibited, as in the case of Germany (Job, 2013). 68

Because the wind power industry is working toward larger turbines capable of producing
10 MW or greater, weight saving is a primary concern because blade mass increases in
proportion to the cube of the rotor radius (Igwemezie et al., 2019). This makes carbon fiber

72 an ideal material because of its high specific stiffness and reduced fatigue sensitivity (Veers et al., 2003). However, the main disadvantage is its high initial cost (Liu and Barlow, 2017). 73 For this reason, carbon-fiber-reinforced polymer (CFRP) has only displaced GFRP in 74 manufacturing structural elements, such as the spar, for blades longer than 45 m. For the next 75 generation of 10 MW units with blades of length 100 m, Wood (2010) notes that the total 76 mass can be reduced by 30% if carbon fiber is used to make blade skins. This mass reduction 77 can potentially mitigate the high cost impact of the material (Veers et al., 2003). Thus, it is 78 recognized that the proportion of carbon fiber composite usage will increase and a trend 79 80 toward fully carbon composite blades is expected (McKenna et al., 2016). Because carbon fibers are energy intensive to produce and have high intrinsic value, there are both 81 environmental and economic motivations for recovering carbon fibers from CFRP (Shuaib et 82 83 al., 2015).

In this study, the concept of Circular Economy (CE) is used to consider how the valuable 84 carbon fiber can be recovered from the end-of-life blades and what economic preconditions 85 are required to allow the fiber to reenter the cycle at the highest possible quality. The CE is 86 defined as "an industrial system that is restorative or regenerative by intention and design. It 87 88 replaces the end-of-life concept with restoration, shifts towards renewable energy, 89 elimination of toxic chemicals which impair reuse and return to the biosphere, and aims for 90 the elimination of waste through the superior design of materials, products, systems, and 91 business models" (Ellen MacArthur Foundation, 2013). The CE creates a closed-loop system in which resources can be kept in a continuous cycle of production and utility, thereby 92 allowing precious and finite resources to generate more value for an extended period of time 93 94 (United Nations Environment Program [UNEP], 2006). Hence, moving toward CE 95 necessitates changes in the way we design, produce, consume, use (and reuse), and manage 96 waste.

Some common CE approaches include: (1) recycling and recovery, where used materials are processed or treated so that they can be reused (Hamzaoui-Essoussi and Linton, 2010); (2) remanufacturing, in which worn-out, damaged, or end-of-life products are restored (Wang and Kuah, 2018); (3) sharing or collaborative consumption for optimization of utility (Belk, 2014); and (4) product life extension, in which products are ultimately designed to have a longer lifetime (Tse et al., 2015). These practices require technological improvements and changes to processes, hence most innovation is driven by industry.

This paper does not consider lifetime extension or collaborative consumption possibilities 104 105 covered by the CE concept, but rather how carbon fiber could reenter the circular economy system at the highest possible quality-either in the forms of a product (reuse/repurpose or 106 107 resize/reshape) or as recycled "raw" or intermediate material (recycle, recovery, and 108 conversion). Sending end-of-life wind turbine blades to landfill is not a long-term viable solution, where many European Union countries legislate against composite waste being sent 109 to landfills (Pickering, 2006). In response, Asmatulu et al. (2013) explored the reuse of these 110 materials as structural components in bridges, buildings, or artificial reefs. Other ways to 111 repurpose blades may involve bridges or urban furniture, but the key challenge remaining in 112 113 the reuse of composites in public amenity infrastructure is to ensure structural integrity. In terms of composite blade recycling, the valuable output streams are fiber, filler, resin, and 114 115 energy recovered (Liu et al., 2019). Blades' recycling typically involves jaw cutters for sectioning before crushing or shredding. Shredding reduces fiber length and strength while 116 hammer milling reduces the composite to smaller fragments, generating noise and dust. The 117 recyclates still contain polymer residue, quality is variable, and applications therefore limited 118 119 to low-grade structures.

From the CE's perspective, material loop needs to be closed and this very much dependson the quality of the recovered carbon fiber and the technicalities involved (Hahladakis and

Iacovidou, 2018; Kasprzyk and Gajewska, 2019). Clean carbon fibers can be recovered 122 through three known thermal decomposition processes. First, a pyrolysis process, which 123 extracts fibers, energy, and pyrolysate at high temperature in an inert environment. The trade-124 off of this process is the use of the lowest possible temperature to devolatilize the polymer to 125 avoid fiber degradation (Fraisse et al., 2016). Second is the "fluidized bed" process 126 (Pickering et al., 2015) to decompose the polymer composite thermally. The feedstock is 127 heated to 450–550 °C on a layer of silica sand, fluidized by a flow of hot air, thereby 128 oxidizing and decomposing the polymer matrix. Solvolysis is an alternative process 129 130 performed using sub- or supercritical fluids. This strips the polymer matrix via a chemical reaction in an aggressive solvent attack. Pure carbon fibers, an inorganic residue, and low 131 molecular weight hydrocarbons are the typical output streams (Sokoli et al., 2018). 132

Among the three recovery options, pyrolysis has been the process of choice in recent 133 decades. Unlike the fluidized bed process technology, which burns off the organic matrix for 134 energy recovery, the pyrolysis process recovers both fiber and a hydrocarbon stream for 135 potential reuse. Although low-cost solvents are used in solvolysis, a high energy intensity of 136 up to 101 MJ/kg (La Rosa et al., 2016) is required to achieve the high pressure and 137 138 temperature conditions, thus limiting their progress to the laboratory scale. In contrast, the energy requirement for a typical pyrolysis process is much lower at around 30 MJ/kg (Witik 139 140 et al., 2013) and compares favorably to virgin carbon fiber production, which consumes 704 141 MJ/kg (Das, 2011). Microwave-assisted heating may also yield energy saving compared with conventional convective furnaces (Jiang et al., 2015). Fiber recovered from the pyrolysis 142 process is relatively clean, with low levels of char residue, and around 90% property retention 143 144 (McConnell, 2010). These fibers also bond well to epoxy resin (Jiang and Pickering, 2016), making them reusable in new composites. 145

146 Despite its growing popularity, few reports address the effect of pyrolysis conditions on the quality of the recovered fiber. Meyer et al. (2009) focused on the effects of pyrolysis 147 temperature, dwell time, and oven atmosphere on the performance of recovered carbon fibers, 148 while Lyon (1998) studied char residuals and their dependence on resin chemistry. A 149 conventional pyrolysis process will result in char formation, which requires a second 150 oxidative treatment (Meyer et al., 2007) because it inhibits free fiber handling and dispersion 151 152 quality in intermediate products such as nonwoven mat (Wong et al., 2012) and compromises adhesion strength. Lower oxidation temperature and short oxidation times seem to assist char 153 154 minimization and fiber strength retention (Yang et al., 2015). Clearly, minimizing char residues is critical, along with minimizing oxidative damage to the fiber. 155

It is evident that carbon fiber recovery from end-of-life blades is a critical issue for 156 greener and more sustainable wind energy production, where successful carbon fiber 157 recovery through pyrolysis is very promising to create and close the circular economy loop. 158 The presence of char residues affects the quality of recovered carbon fibers and posttreatment 159 processes are needed, which add additional cost and complexity to the recovery of fibers. To 160 achieve this, we determine the pyrolysis conditions that lead to ideal recovered fibers, which 161 162 could reenter the circular economy system at the highest possible quality and without any secondary cleaning. 163

Hence, this paper investigates the potential of CFRP recovery and the quality of the recovered materials. To close the CE loop, the technicalities and economics of extraction are considered, alongside the potential applications of recovered fibers. The paper is organized as follows: Section 2 presents the method to determine the pyrolysis conditions that lead to ideal recovered fibers, which could reenter the circular economy system at the highest possible quality. Section 3 presents the results; while Section 4 discusses the recovery costs, economic preconditions, and considerations for fiber applications. Section 5 concludes.

171 **2.** Methodology

The effects of pyrolysis temperature, heating rate, and nitrogen flow rate on char volume were investigated using a thermogravimetric analyzer (TGA). Then, the oxidation rate of the produced char, as expressed in terms of intrinsic reactivity, was measured via a nonisothermal approach. The morphology of the char was then studied via a scanning electron microscopy (SEM) analysis.

177 2.1 Materials

Unidirectional prepreg Toray® T700s carbon fibers and 37 wt% epoxy resin were
supplied by Aojing Composite Company, Shanghai, China. The prepreg was cut to 200 mm
by 200 mm and cured at 140 °C in air for 2 h. The release film and backing paper were
removed before the prepreg was pyrolyzed using a TGA. To study the char oxidation rate,
epoxy was squeezed out from the as-received prepreg between hot platens at 5 MPa and 80
°C. The resin was cured at the previous schedule and subjected to thermal analysis, as
described below.

185 2.2 Thermal analysis

Thermal and degradation properties of the cured prepreg were investigated using an SDT 186 Q600 TGA from TA Instruments, Delaware, US, on approximately 20 mg samples in a 187 nitrogen environment according to the heating profiles summarized in Fig. 2. Samples were 188 heated from ambient to either 550 °C or 650 °C, after which the samples were held 189 isothermally for 30 min before cooling to room temperature. A range of heating rates were 190 used in this study. The slowest heating rate was decided according to the common practice in 191 lab-scale pyrolysis studies on composite waste, which is between 10 and 30 °C/min 192 (Onwudili et al., 2016; Song et al., 2017), thus it was set to 20 °C/min. The highest heat rate 193 was determined by the capability of the TGA unit, i.e., 200 °C/min. Other selected heating 194 rates were 80 and 100 °C/min, which are common in fast pyrolysis studies on biomass (Wang 195

et al., 2019) and coal (Jiang et al., 2019). The weight loss profile of the degrading sample
under these four different heating rates was recorded. These tests were undertaken at a
constant nitrogen gas flow rate of 50 ml/min. However, in the later stage of the study, the
nitrogen gas flow rate was increased to 100, 200, and 400 ml/min with other process
variables unchanged.

201

----- INSERT FIGURE 2 HERE -----

202 Char oxidation kinetics was studied by subjecting the neat epoxy to the same thermal 203 cycles as shown in Fig. 3 to create different grades of char. The gas flow was maintained at 204 50 ml/min. The pyrolytic chars were later dried and subjected to an intrinsic reactivity test 205 and SEM analysis, as detailed below.

206 2.3 Char analysis

207 The combustion characteristics of carbonaceous residue were determined using an intrinsic reactivity analysis with nonisothermal heating in air (Unsworth et al., 1991). 208 209 Pyrolytic char samples were heated from ambient temperature to 105 °C inside an air-filled 210 chamber at a heating rate of 20 °C/min. The temperature was maintained for 30 min for moisture removal and then ramped to 900 °C at the same heating rate to complete the 211 intrinsic reactivity study. Mass loss profile (TG) and the first derivative of the mass loss 212 profile (DTG) were analyzed to identify peak temperature (PT) and burnout temperature (BT) 213 of the pyrolytic char sample. The peak of the DTG curve was used to determine the PT value 214 because it is defined as the temperature at which the highest combustion rate occurs. The BT 215 is defined at 1 wt%/minute of combustion rate. A Zeiss@ Sigma VP scanning electron 216 microscope was used to study the morphology of pyrolytic char with a 10 kV accelerating 217 218 voltage.

219 **3. Results**

220 3.1 Effects of heating rates and pyrolysis temperatures

221 TGA mass loss profiles are shown in Fig. 4, which clearly demonstrate that after a marginal drop during early-stage heating, each of the profiles undergoes a sharp drop in mass 222 223 before finally reaching a plateau region. The initial drop was mainly due to moisture loss, while conversion of the epoxy matrix into volatiles produced the sharp loss in mass and the 224 225 rate of conversion, which is accelerated at higher pyrolysis temperatures. A portion of the epoxy matrix was converted into pyrolytic char and remained on the surface of the carbon 226 fiber. Together, they contributed to the final masses at the plateau region as shown in Fig. 3, 227 which vary with heating rates and pyrolysis temperatures. Because the carbon fiber 228 229 reinforcement was relatively unaffected by the pyrolysis process, the variations in final mass loss corresponded to the extent of char retention. 230

231

----- INSERT FIGURE 3 HERE -----

The variations in mass loss are further illustrated in Fig. 5, recalling the initial epoxy 232 233 loading of 36.4 wt%. A mass loss exceeding 36.4 wt% suggests degradation of the carbon fiber, but a lower value indicates the presence of pyrolytic char. At 550 °C, a mass loss of 234 28.0 wt% was recorded at 20 °C/min and a further 5 wt% reduction was achieved by ramping 235 236 the heating rate to 200 °C/min, which suggested the fiber residue entrained 3.5 wt% of char. Lower char contents were obtained at the higher pyrolysis temperature of 650 °C and again, 237 higher heating rates resulted in greater mass loss, but the rate effects were lower than that at 238 550 °C. Bridgwater and Peacocke (2000) have reported the significance of these two factors 239 on the mass distribution of char and volatiles from biomass, typically a higher heating rate 240 241 and pyrolysis temperature favored the production of gaseous products and the reverse conditions favored char formation due to secondary coking and repolymerization reactions. 242 These agree with the findings reported in Fig. 4, and because the aim of the project is to 243

reduce char formation, this can be achieved with higher heating rate and/or increasing the
pyrolysis temperature from 550 °C to 650 °C. The former factor is preferable because higher
temperatures are likely to degrade the carbon fiber performance.

247

----- INSERT FIGURE 4 HERE -----

248 3.2 Effect of nitrogen gas flow rate

Fig. 5 shows the mass loss curve for prepreg at different nitrogen gas flow rates for two 249 different pyrolysis temperatures. It can be seen in Fig. 5(a) that at a pyrolysis temperature of 250 550 °C, more volatiles were released, or fewer char residues were left on the fiber when the 251 gas flow rate was increased from 50 ml/min to 200 ml/min for both 20 °C/min and 80 °C/min 252 heating rates. Higher flow rate suggests shorter residence time within the heating chamber for 253 254 volatiles and this reduces secondary reactions that promote char formation (El-Harfi et al., 255 1999; Pütün et al., 2006; Uzun et al., 2007) or cracking of the primary volatiles and repolymerization in hot char particles (Lanzetta et al., 1997). However, no further significant 256 mass loss was observed with gas flow rate higher than 200 ml/min. In contrast, the 257 dependency of mass loss on gas flow rate became less extensive at a heating rate above 100 258 °C/min. Previous studies again support this finding, e.g., a shortened volatiles' residence time 259 was observed by Montoya et al. (2015) in depolymerization reactions of cellulose and 260 hemicellulose. In another case, which focused on pyrolytic behavior of rapeseed, Havkiri-261 Acma et al. (2006) found that a higher heating rate reduced volatiles' residence time, which 262 could further reduce secondary reactions such as cracking, repolymerization, and 263 recondensation. Our results are consistent with these studies because greater mass loss 264 accompanied higher heating rates and the volatiles' residence time was expected to be greatly 265 reduced and become independent of nitrogen flow rate for a heating rate above 100 °C/min. 266

267 Similar tests on the effect of gas flow rate were repeated at a higher pyrolysis temperature of 650 °C. However, as plotted in Fig. 5(b), a rather complex relationship is observed. At 20 268 269 and 80 °C/min heating rates, char mass loss increased gradually to 32.4% and 33.6%, respectively, with increasing gas flow rate to 200 ml/min, but the mass loss started to decline 270 with further increase in flow rate to 400 ml/min. A general trend toward higher mass loss, 271 despite not being as evident as the results at 550 °C, can be identified for 100 and 200 °C/min 272 heating rates. Overall, the impact of the gas flow rate was less apparent at 650 °C. 273 ----- INSERT FIGURE 5 HERE -----274 Intrinsic reactivity analysis of char oxidation rate 275 3.3 Fig. 6 shows the effects of pyrolysis temperature and heating rate on chars' intrinsic 276 277 properties; at either 550 °C or 650 °C, both PT and BT reduce with higher heating rates, which indicates char resulting from higher heating rate was more reactive and could be 278 279 oxidized at a lower temperature. In addition, higher pyrolysis temperatures increased the BT value provided the heating rate was less than 100 °C/min. Consistent with this, Chitsora et al. 280 (1987) reported such an effect in relation to German bituminous coal char produced in a 281

fluidized bed, similarly on lignite char by Ashu et al. (1978).

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284 3.4 Scanning electron microscopy

The effects of heating rates and pyrolysis temperatures on the morphologies of pyrolytic char are depicted in SEM images shown in Fig. 7. It is evident that the combination of low heating rate and low pyrolysis temperature, as shown in Fig. 7(a), created char with a rough but continuous appearance. However, at 650 °C, as shown in Fig. 7(b), porosity became apparent, increasing with higher temperature and heating rate. Fushimi et al. (2003) suggested that a high heating rate caused a rapid evolution of volatiles, which in turn increased the porous structure. Fast volatile release rate produced considerable overpressure,
which encouraged void coalescence and greater porosity levels (Guerrero et al., 2005).
Septien et al. (2018) reported that a high porosity level would enhance gas species diffusion
within the char open structure, which facilitated penetration of oxygen and better evacuation
of reaction products from the porous structure. Char created from the epoxy matrix in this
study reinforced their findings because a high intrinsic reaction was found from char with a
high porosity.

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----- INSERT FIGURE 7 HERE -----

299 **4. Discussion**

Section 3 reported that a rapid heating rate caused a substantial reduction of pyrolytic 300 301 char volume, particularly for pyrolysis at 550 °C. The inert-gas flow rate was another contributing factor to char yield and the level at which it affected the char content depended 302 on the pyrolysis temperature and heating rate. Higher gas flow rate promoted devolatilization 303 304 and reduced the char content provided the heating rate was less than 100 °C/min and the pyrolytic temperature was 550 °C. However, the positive effect became insignificant at 305 higher temperature and heating rate. The intrinsic reactivity of the char was significantly 306 307 influenced by the pyrolytic reaction conditions. Char with higher intrinsic reactivity was associated with high heating rates and temperature and this implied the char had a faster 308 oxidation rate. These findings are of commercial relevance to the carbon fiber recycling 309 industry with high priority in cost control because with a lower char volume and faster 310 oxidation kinetics, the energy-intensive oxidation process can be shortened and the carbon 311 fiber can potentially be recovered with a higher mechanical performance due to the 312 compressed thermal cycle. The importance of recovery cost and the reuse options available 313 for the recovered carbon fiber will be discussed in subsequent sections. 314

315 4.1 Recovery costs

Presently, there is no industrial-scale recycling of end-of-life turbine blades; therefore, the 316 costs and actual commercialization procedure have not been well-defined (Larsen, 2009). 317 Research on recycling and remanufacturing of these items is still ongoing. Pyrolysis is a 318 mature fiber recovery approach and has been considered suitable for mass-scale commercial 319 efforts use (Rybicka et al., 2016). Existing pyrolysis practices require size reduction and 320 321 progressively shorter fibers (and lower value) as the number of cycles increases. Thus, the hierarchy of applications ranges from initial, continuous fiber composites, ultimately to 322 323 milled fiber fillers for lower grade structures. This potential circular economy flow is illustrated in Fig. 8. 324

325

----- INSERT FIGURE 8 HERE -----

The materials CE loop sets some economic preconditions for the retrieval of carbon fibers. At the initial stages, without a demand-side pull, legislative drivers, or standards in the reuse of materials, private sector investments are unlikely. Furthermore, implementing recycling and recovery comes at a price, including the collection costs, pretreatment and sorting costs, and the costs of final recovery.

However, the market value of the recovered carbon fiber and concomitant by-products 331 could offset many of these costs. This is because the production process of virgin carbon 332 333 fibers is energy intensive, and incurs high manufacturing cost, especially in the case of highgrade carbon fiber (used for structural applications such as blades). Therefore, there is a 334 greater economic incentive to recover these carbon fibers. Moreover, the costs of 335 336 commercially available fibers reclaimed through pyrolysis have been reported by industry sources to be about 10 Euros per kg while the market value of virgin product is 18–50 Euros 337 per kg (ELG Carbon Fiber, 2016). 338

Industry perspectives also agree that the cost to recover carbon fiber will be a fraction of that for producing virgin carbon fiber (Carberry, 2008). The energy requirement to recover carbon fibers (Cherrington et al., 2012; Vo Dong et al., 2018) is typically <10% that of virgin fiber production¹. Previous studies also highlighted the importance of throughput in reducing the unit cost through a recycling plant (Meng et al., 2018). Clearly, the energy requirements, efficiency, and cost associated with recycling the carbon fibers from blades would improve beyond the current reported (laboratory) figures in mature, mass production settings.

346 4.2 Economic preconditions needed

As the technology for recovery and up-scaling of recycling continues to be developed,
there are four considerations that need to be addressed to enable the takeoff and growth in the
recovery of carbon fibers from end-of-life blades.

First, there must be a network to ensure a consistent supply of feedstock for fiber recovery that would deliver economies of scale. The current lack of infrastructure for collecting end-of-life blades is a key challenge. Ideally, recycling facilities should be located close to wind farms; alternatively, mobile recycling units have been trialed in some regions. Sorting and classification will also improve value streams. Nonstandard construction (Brøndsted et al., 2005) means that traceability would help to identify ideal processing parameters, likely yield, etc.

Second, a marketplace must be created for secondary or recovered materials (Stahel,
2013) to centralize demand for recyclates or fibers produced. The market demand for the
materials will help to offset the cost of decommissioning and collecting end-of-life blades.
The concept of CE necessitates that there is a ready market to receive and reintroduce the
recovered materials into the economic cycle (Wang and Kuah, 2018). There could be an issue

¹286 MJ/kg (Suzuki and Takahashi, 2005) and 704 MJ/kg (Das, 2011)

if the cost of virgin materials is already low as in the case of glass fibers. The recovered
materials must have a value higher than the cost needed to retrieve them, i.e., using recovered
fibers must be cheaper than the cost of using virgin materials directly. This is the most likely
case for carbon fibers.

The recent agreement in providing composite waste from Boeing's aircraft manufacturing 366 367 facilities to ELG Carbon Fiber signaled both the value of composite waste supply and the availability of a marketplace for the recovered fiber (Zazulia, 2018). Fiber recovered from the 368 manufacturing wastes and growing end-of-life parts can potentially help in mitigating the 369 370 shortage in virgin fiber supply, particularly in the demand for discontinuous fibers. Recyclers have been developing scalable conversion technologies to enlarge the supply-side capacity 371 for recovered fiber. For example, a new hybrid nonwoven mat containing recovered carbon 372 373 fiber and polyamide 6 resin was developed for making seatbacks for the high-volume automotive applications (Milberg, 2017). Driven by the affordability (Nicolais and Pisanova, 374 2012) and more environmentally friendly recovery process, more reuse applications in the 375 near future are anticipated. 376

Third, quality standards for the fibers or recyclates must be established to build confidence (Carberry, 2008; Finnveden et al., 2013; Job, 2013; Pickering, 2006; Wood, 2010). The design of a product, the material retrieval system, efficiency of sorting, and the recovery technology are fundamental in increasing the quantity, quality, and usability of recovered materials (Gregson et al., 2015).

Fourth, key legislation and government policy intervention need to mandate both operators and end-users into the reuse of recovered carbon fiber with accompanying fiscal penalties and benefits. Cherrington et al. (2012) outlined some of the key examples of legislation and directives relevant to end-of-life blades. Landfill and incineration disposal are increasingly penalized (Cherrington et al., 2012) whilst R&D incentives for sustainable
product design and technologies that enhance the recycling process (Söderholm and Tilton,
2012) are increasingly important. Extended Producer Responsibility (EPR) is another
important initiative to encourage further recycling, where producers play a more proactive
role in supporting recovery and reuse. EPR has been successfully utilized for end-of-life
vehicles and waste electrical and electronic equipment (Cherrington et al., 2012).

392 4.3 Recovered carbon fibers' applications and considerations

393 Low-grade application:

Granulation of CFRP scrap requires the lowest energy of all recovery methods (Wong et
al., 2017). These recyclates can be sorted into resin-rich and fibrous-rich groups, but both
have low commercial value because the recyclates still contain a high level of resin residues,
limiting their usage to low-grade applications, such as being used as a filler for polymer resin
or construction materials (Thomas et al., 2014) and concrete (Mastali and Dalvand, 2016).

399 Medium-grade application:

400 To maximize the value of recovered carbon fibers, they should be separated from the polymer matrix and the fiber should retain enough mechanical performance for the next 401 application. To date, this can be achieved via the common pyrolysis process and with the use 402 403 of adequate pyrolytic conditions; as discussed in this paper, cleaner and stronger carbon fibers can potentially be recovered. However, blades are bulky, and to reduce logistical cost, 404 405 decommissioned blades are sectioned in situ to a manageable size for transportation to recycling facilities, at which, further size reduction has taken place prior to feeding to the 406 pyrolysis process. 407

408 As a result, the recovered fibers are generally short and fluffy and cannot be processed in 409 the same way as the virgin fibers. To allow the fibers to reenter the circular economy system at the highest possible quality, they should be converted into intermediate forms suitable forindustrial molding processes.

Nonwoven mat is a common intermediate form widely offered by the recycling 412 industries, which can be made by carding and spinning or papermaking. Both are cost-413 effective processes, suited to mass volume production and with versatile combinations of 414 thermoplastic filaments or powders suitable for thermoforming (Wolling et al., 2017). 415 Because of the random orientation of fibers, the fiber packing density is limited to around 416 30% (Wong et al., 2017). Nonwovens are typically used in nonstructural applications, such as 417 tooling for aerospace parts (Gardiner, 2014), heating elements (Pang et al., 2012), and 418 electromagnetic interference shielding (Wong et al., 2010). 419

420 Higher-grade application:

421 Fiber alignment is a necessary intermediate step for higher-value applications because the presence of a close-packed structure greatly increases the reinforcing potential of the 422 fibers. Hydrodynamic alignment was originally developed in the 1970s (Bagg et al., 1977) 423 but more recent innovations (e.g., van de Werken et al., 2019; Wong et al., 2009) optimize 424 streamline velocities to deposit an aligned fiber slurry onto a moving mesh. Clean, free-425 426 flowing filaments are essential here, underlining the need for a char-free feedstock, because char carryover inhibits uniform dispersion, hence the need for upstream control of pyrolytic 427 conditions, as reported here. 428

Other alignment technologies include electrostatics (Ravindran et al., 2018), air streaming
(Ericson and Berglund, 1993), and the dry carding process (Miyake and Imaeda, 2016). Fiber
alignment plays an important role in upgrading the value of the recovered carbon fiber but,
clearly, production economics remains to be established for any of these secondary

433 operations.

434 **5.** Conclusions and Recommendations

This paper is the first to consider urban mining of carbon fiber from end-of-life wind
turbine blades to close the CE loop. Using the concept of CE in reusing, repurposing,
recycling, and recovering, this paper investigates CFRP recovery and the quality of the
recovered materials.

439 Our investigation revealed that pyrolytic reaction conditions were important in controlling char formation volume and its oxidation rate. A rapid heating rate caused a substantial 440 reduction of pyrolytic char volume, particularly for the pyrolysis process undertaken at 550 441 °C. Nitrogen gas flow rate also affected the char content at a specific combination of 442 pyrolysis temperature and heating rate. At 550 °C and less than 100 °C/min heating rate, a 443 higher gas flow rate favored the devolatilization process and reduced the char content. High 444 445 heating rate and pyrolysis temperature produced char with higher intrinsic reactivity, suggesting a faster oxidation rate. This is beneficial to shorten the post-processing step, 446 thereby leading to lower energy costs. These findings are of commercial significance to the 447 carbon fiber recycling industry with high priority in cost control as with lower char volume 448 and faster oxidation kinetics, and hence the carbon fiber can potentially be recovered with a 449 450 higher mechanical performance due to the shortened thermal cycle.

Creating a market and closing the CE loop requires several issues to be overcome so that 451 452 recovered carbon fibers can be accepted as an environmentally friendly, reliable, and costeffective material. The industry would require establishment of standards for the recycled 453 carbon fiber products and to regulate pyrolysis operations. In addition, a labeling scheme 454 such as those used in recycled plastics would yield greater user acceptance and support. This 455 addresses the demand-side conditions. Further fiscal incentives and penalties by governments 456 would also push the supply side so that companies might engage more responsibly in closing 457 the circular loop. 458

459 Our investigation also identifies scope for future studies. This investigation looked into maximum carbon recovery for first-time recycled carbon fiber. Carbon fiber physical and 460 mechanical properties will degrade over time after multiple thermal treatments, hence 461 affecting their reuse value. Therefore, a more detailed study is recommended to encompass 462 this complex scenario of having different stages of recovered fiber content to ensure long-463 term sustainability. Second, the thermal pyrolysis of carbon fiber produces two other by-464 products-oil and gas-that have good calorific and some economic value. Clearly, further 465 study of these by-products would assist a full loop recycling solution for the composite 466 467 wastes.

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A circular economy approach to green energy: Wind turbine, waste, and

material recovery



Figure 1: Annual new wind turbine installations by region

Source: Adapted from Liu and Barlow (2017)



Figure 2. Thermal treatment profile used in TGA test



Figure 3. Effect of heating rates and pyrolysis temperatures on CFRP's TG curves

Figure 4: Effect of heating rates and pyrolysis temperatures on CFRP's mass loss









Figure 6. Effect of heating rates on intrinsic reactivity of char generated at 550 and 650 °C.

Figure 7. SEM images of pyrolytic chars produced at different temperatures and heating rates (a) 550°C, 20°C/min (b) 650°C, 20°C/min (c) 550°C, 200°C/min and (d) 650°C, 200°C/min





Figure 8. Circular economy for end-of-life wind turbine blades